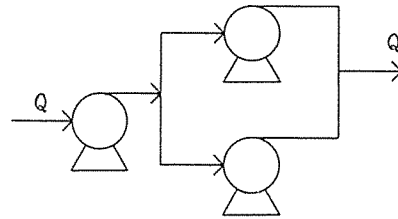


Problem 1 (20 points)

- (a) Navier-Stokes equation is a mathematical statement of a physical principle. What is the principle? (3 points)
- (b) The “operating line” used in the calculations of many separation processes is a graphical presentation of a physical principle. What is the principle? (3 points)
- (c) Three identical centrifugal pumps are connected as shown in the figure. The head increase across a single such pump varies with the flow rate Q as: $\Delta h = a + bQ^2$. Here a and b are constants. Calculate the head increase in the arrangement shown in the right figure in terms of a , b and Q . (4 points)
- (d) Please define the “effectiveness, ϵ ” used in the heat exchanger design and calculations. (3 points)
- (e) Please define the Biot number (Bi) and Nussult number (Nu), and comment on the differnece between them. (4 points)
- (f) Please describe the difference between the “free convection” and “forced convection” (3 points)



Problem 2 (25 points)

We consider a Newtonian liquid with uniform velocity v_∞ past a spherical bubble of radius R filled with air at creeping flow condition. The velocity and pressure field around the bubble has been solved as follows:

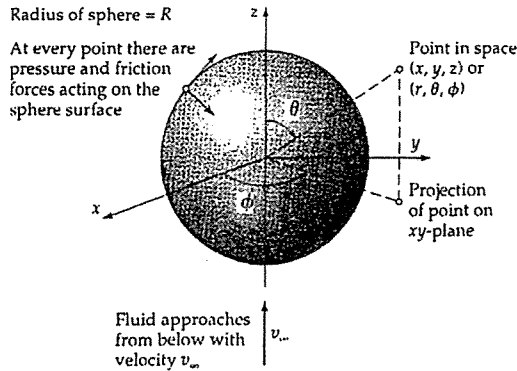
$$v_r = v_\infty \left[1 - \left(\frac{R}{r}\right) \right] \cos\theta, \quad v_\theta = -v_\infty \left[1 - \frac{1}{2}\left(\frac{R}{r}\right) \right] \sin\theta, \quad v_\phi = 0$$

$$p = p_0 - \rho g r \cos\theta - \left(\frac{\mu v_\infty}{R}\right) \left(\frac{R}{r}\right)^2 \cos\theta$$

Here p_0 is the pressure very far from the bubble.

- (a) We want to derive the equation of drag force acting on the bubble. Please indicate which stress components (Ex: $\tau_{\phi r}$) are relevant to this derivation and obtain their formula using the velocity field. (6 points)
- (b) Determine the drag force exerted on the bubble? Remember to include the pressure contribution. (10 points)
- (c) Determine the drag coefficient C_D of the bubble at this condition. (4 points)

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(d) The result in (c) is somewhat different from Stokes' law. What causes this difference? If you do not have the answer for (c), make a guess and explain your reason. (5 points)

Newton's law of viscosity for incompressible fluid in spherical coordinates:

$$\tau_{rr} = -\mu \left[2 \frac{\partial v_r}{\partial r} \right]$$

$$\tau_{\theta\theta} = -\mu \left[2 \left(\frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r}{r} \right) \right]$$

$$\tau_{\phi\phi} = -\mu \left[2 \left(\frac{1}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} + \frac{v_r + v_\theta \cot \theta}{r} \right) \right]$$

$$\tau_{r\theta} = \tau_{\theta r} = -\mu \left[r \frac{\partial}{\partial r} \left(\frac{v_\theta}{r} \right) + \frac{1}{r} \frac{\partial v_r}{\partial \theta} \right]$$

$$\tau_{\theta\phi} = \tau_{\phi\theta} = -\mu \left[\frac{\sin \theta}{r} \frac{\partial}{\partial \theta} \left(\frac{v_\phi}{\sin \theta} \right) + \frac{1}{r \sin \theta} \frac{\partial v_\theta}{\partial \phi} \right]$$

$$\tau_{\phi r} = \tau_{r\phi} = -\mu \left[\frac{1}{r \sin \theta} \frac{\partial v_r}{\partial \phi} + r \frac{\partial}{\partial r} \left(\frac{v_\phi}{r} \right) \right]$$

Problem 3 (15 points)

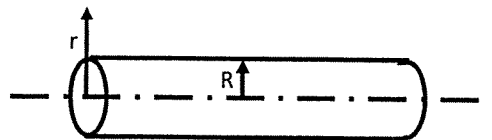
It is desired to separate a binary mixture by simple distillation. If the feed mixture has a composition of 0.5 mole fraction, and the distillate has a composition of 0.75 mole fraction, calculate the fraction which it is necessary to vaporize. The equilibrium curve is given by: $y = 1.2x + 0.2$.

(a) Use a flash distillation process. (5 points)

(b) Use a differential distillation process. (10 points)

Problem 4 (25 points)

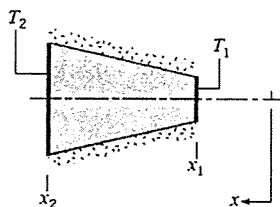
Gas A diffuses through a stagnant gas film to the surface of a nonporous cylindrical catalyst, where it undergoes the chemical reaction: $2A \rightarrow B$ (the reaction rate constant = k). Gas B then diffuses from the surface of the catalyst and is swept away. If the diffusion and reaction on the ends of the particle are neglected and the temperature, diffusion coefficient D_{AB} , and total concentration C remain constant. Consider this a steady-state operation and one-dimensional (r -direction) mass transfer (see the figure below), please answer the following questions:



- (a) What is the unit of the “reaction rate constant k ”? (3 points)
- (b) What is the unit of the “molar flux of A”? (3 points)
- (c) Please show your results after performing the “shell mass balance” on both species A and B. (6 points)
- (d) $N_{Ar} = \square N_{Br}$ at $r = R$ (the catalyst surface), what is \square ? Please also give the reason why this stoichiometry relationship stays true at any r . (5 points)
- (e) If the chemical reaction at the surface is very fast, and $y_A = y_{A\delta}$ at $r = \delta R$, please derive an equation for the molar flux of A. (8 points)

Problem 5 (15 points)

The figure shown below is a conical section fabricated from pyroceram. It is of circular cross section with the diameter $D = ax$, where $a = 0.25$. The small end is at $x_1 = 5$ cm and the large end at $x_2 = 25$ cm; the end temperatures are $T_1 = 400$ K and $T_2 = 600$ K. If the lateral surface is well insulated, no heat generation is involved, steady-state condition is considered, and all properties are assumed constant. Please answer the following questions:



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- (a) Starting from the "equation of conservation of energy" or "energy balance equation", please explain the reason why the heat transfer rate q_x is independent of x . (4 points)
- (b) Derive an expression for the temperature distribution $T(x)$ in symbolic form, assuming one-dimensional conditions. Sketch the temperature distribution. (7 points)
- (c) Determine the heat transfer rate, q_x , through the cone. (4 points)

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